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75	90 09/28/2005		EXAMINER		
John E. Vick, Jr.			STAICOVIC	STAICOVICI, STEFAN	
Legal Departme M-495	ent		ART UNIT	PAPER NUMBER	
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Spartanburg, SC 29304			DATE MAILED: 09/28/2005	DATE MAILED: 09/28/2005	

Please find below and/or attached an Office communication concerning this application or proceeding.

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		Application No.	Applicant(s)	
Office Action Summary		10/764,234	BATLAW ET AL.	
		Examiner	Art Unit	
	_	Stefan Staicovici	1732	
Period fo	The MAILING DATE of this communication app or Reply	ears on the cover sheet with the c	orrespondence addres	:s
A SH WHIC - Exte after - If NC - Failt Any	ORTENED STATUTORY PERIOD FOR REPLY CHEVER IS LONGER, FROM THE MAILING DANSIONS of time may be available under the provisions of 37 CFR 1.13 SIX (6) MONTHS from the mailing date of this communication. Depriod for reply is specified above, the maximum statutory period vire to reply within the set or extended period for reply will, by statute reply received by the Office later than three months after the mailing ed patent term adjustment. See 37 CFR 1.704(b).	ATE OF THIS COMMUNICATION 36(a). In no event, however, may a reply be tim will apply and will expire SIX (6) MONTHS from a cause the application to become ABANDONE	N. nely filed the mailing date of this commu D (35 U.S.C.§ 133).	
Status				
1)⊠ 2a)□ 3)□	Responsive to communication(s) filed on <u>13 Ju</u> This action is FINAL . 2b) This Since this application is in condition for allowar closed in accordance with the practice under E	action is non-final. nce except for formal matters, pro		rits is
Disposit	ion of Claims			
considera 5)	Claim(s) is/are allowed. Claim(s) <u>1-8,13,14,16-22,25-27,30,32-37,39,4</u>	19, 31, 38, 40, 43-44, 47-48 and 5 1,42,45,46 and 49 is/are rejected r election requirement. r. epted or b) □ objected to by the I drawing(s) be held in abeyance. See ion is required if the drawing(s) is objected	Examiner. e 37 CFR 1.85(a). jected to. See 37 CFR 1	.121(d).
Priority ı	under 35 U.S.C. § 119		•	
12)□ a)i	Acknowledgment is made of a claim for foreign All b) Some * c) None of: 1. Certified copies of the priority document: 2. Certified copies of the priority document: 3. Copies of the certified copies of the priority document: application from the International Bureau See the attached detailed Office action for a list	s have been received. s have been received in Applicati rity documents have been receive u (PCT Rule 17.2(a)).	on No ed in this National Sta	ge
2) 🔲 Notic 3) 🔯 Infor	et(s) ce of References Cited (PTO-892) ce of Draftsperson's Patent Drawing Review (PTO-948) mation Disclosure Statement(s) (PTO-1449 or PTO/SB/08) er No(s)/Mail Date 1/23/04	4) Interview Summary Paper No(s)/Mail Di 5) Notice of Informal F 6) Other:		2)

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DETAILED ACTION

Election/Restrictions

1. Applicant's election of Group I, Species A in the reply filed on June 14, 2005 is acknowledged. Because applicant did not distinctly and specifically point out the supposed errors in the restriction requirement, the election has been treated as an election without traverse (MPEP § 818.03(a)).

Claim Rejections - 35 USC § 103

- 2. The following is a quotation of 35 U.S.C. 103(a) which forms the basis for all obviousness rejections set forth in this Office action:
 - (a) A patent may not be obtained though the invention is not identically disclosed or described as set forth in section 102 of this title, if the differences between the subject matter sought to be patented and the prior art are such that the subject matter as a whole would have been obvious at the time the invention was made to a person having ordinary skill in the art to which said subject matter pertains. Patentability shall not be negatived by the manner in which the invention was made.
- 3. Claims 1-5, 16, 19-22 and 25 are rejected under 35 U.S.C. 103(a) as being unpatentable over Sato (US Patent No. 3,944,643) in view of Edwards (US Patent No. 3,966,382).

Sato ('643) teaches the basic claimed process of injection stretch blow molding of a polypropylene container including, providing a polypropylene based composition having a melt flow index of 7 g/10 min, injecting said composition into a mold to form a preform and removing said preform to be blow molded in a subsequent molding step (see Abstract and col. 5, lines 64-67).

Regarding claim 1, Sato ('643) does not teach a mold fill rate of at least 5 g/sec. However, it is noted that it is well known that the mold fill rate is dependent on the injection

pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence it is submitted that the mold fill rate is a result effective variable. Therefore, it would have been obvious for one of ordinary skill in the art to have used routine experimentation in the process of Sato ('643) to determine an optimum mold fill rate of at least 5 g/sec because it is well known that the mold fill rate is dependent on the injection pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence the mold fill rate being a result effective variable.

Further regarding claim 1, Sato ('643) does not teach a preform wall thickness of less than 3.5 mm. Edwards ('382) teaches that the wall thickness of a polypropylene preform used in an injection-blow molding process is 0.02 inches (0.5 mm) (see col. 1, line 57 through col. 2, line 15). Therefore, it would have been obvious for one of ordinary skill in the art to have molded a polypropylene preform having a wall thickness of 0.5 mm (less than 3.5 mm) as taught by Edwards ('382) using the process of Sato ('643) because Edwards ('382) specifically teaches that such a value provides for a highly accurate end-product, hence providing for an improved product.

In regard to claim 2, Sato ('643) teaches reheating and stretch-blow molding of the preform to form a container (see Abstract).

Specifically regarding claim 3, although Sato ('643) in view Edwards ('382) teaches a polypropylene preform wall thickness of 0.5 mm, Sato ('643) in view Edwards ('382) does not teach a polypropylene preform wall thickness of 1.5-3.5 mm. However, Edwards ('382) teaches that the preform wall thickness depends on the type of resin, heating temperature, injection

pressure. Hence, it is submitted that in view of the teachings of Edwards ('382), it would have been obvious for one of ordinary skill in the art to have used routine experimentation to determine an optimum wall thickness in the process of Sato ('643) in view Edwards ('382) because, Edwards ('382) teaches that the preform wall thickness depends on the type of resin, heating temperature, injection pressure, hence teaching that the preform wall thickness is a result effective variable.

Regarding claim 4, Sato ('643) in view Edwards ('382) does not teach a mold fill rate of 5-22 g/sec. However, it is noted that it is well known that the mold fill rate is dependent on the injection pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence it is submitted that the mold fill rate is a result effective variable. Therefore, it would have been obvious for one of ordinary skill in the art to have used routine experimentation in the process of Sato ('643) to determine an optimum mold fill rate of 5-22 g/sec because it is well known that the mold fill rate is dependent on the injection pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence the mold fill rate being a result effective variable.

In regard to claim 5, Sato ('643) teaches an ethylene-propylene co-polymer (see col. 6, lines 23-24).

Specifically regarding claim 16, Sato ('643) teaches a polypropylene polymer (homopolymer).

Regarding claim 19, Edwards ('382) teaches a mold gate of about 3 mm (see Figures 2-3).

In regard to claims 20-22, it is noted that the productivity of a molding process is dependent on the material being processed and the molding parameters, hence being a result effective variable. Therefore, it would have been obvious for one of ordinary skill in the art to have used routine experimentation in the process of Sato ('643) in view of Edwards ('382) to determine an optimum production rate because it is well known that the productivity of a molding process is dependent on the material being processed and the molding parameters, hence being a result effective variable.

Specifically regarding claim 25, it is submitted that the container of Sato ('643) in view of Edwards ('382) has a haze ratio of less than about 0.05 haze/mils because the same materials and process are being used as claimed in the instant invention and as such the resulting molded container has the same properties.

4. Claim 6-8 and 17-18 are rejected under 35 U.S.C. 103(a) as being unpatentable over Sato (US Patent No. 3,944,643) in view of Edwards (US Patent No. 3,966,382) and in further view of Schmidt *et al.* (US2004/0063830 A1).

Sato ('643) in view Edwards ('382) teach the basic claimed process as described above.

Regarding claims 6-8 and 13-14, Sato ('643) in view Edwards ('382) do not teach the use of a nucleating agent. However, the use of a nucleating agent to improve the transparency of the polypropylene molded container is well known as evidence by Schmidt *et al.* (US2004/0063830 A1) who teaches the use of DBS as a nucleating agent, specifically 1,3-2,4-dimethylbenzylidene (see paragraph [0004]). Therefore, it would have been obvious for one of ordinary skill in the art to have provided DBS as a nucleating agent as taught by Schmidt *et al.* (US2004/0063830 A1) in

the process of Sato ('643) in view Edwards ('382) because, Schmidt *et al.* (US2004/0063830 A1) teaches that DBS (nucleating agent) provides for improved transparency, hence providing for an improved product.

In regard to claims 17-18, although Sato ('643) in view Edwards ('382) teach a polypropylene (homopolymer) composition, Sato ('643) in view Edwards ('382) do not specifically teach a polypropylene random copolymer or a polypropylene block copolymer. Schmidt *et al.* (US2004/0063830 A1) teaches that a polypropylene homopolymer, a random copolymer or a polypropylene block copolymer are equivalent alternatives as injection blow molding materials (see paragraph [0011]). Therefore, it would have been obvious for one of ordinary skill in the art to have provided a random copolymer or a polypropylene block copolymer as an equivalent alternative to a polypropylene homopolymer as taught by Schmidt *et al.* (US2004/0063830 A1) in the process of Sato ('643) in view Edwards ('382) because, Schmidt *et al.* (US2004/0063830 A1) teaches that a polypropylene homopolymer, a random copolymer or a polypropylene block copolymer are equivalent alternatives as injection blow molding materials.

5. Claims 26-27, 32-37, 39, 41-42, 45-46 are rejected under 35 U.S.C. 103(a) as being unpatentable over JP 60-125627 in view of Edwards (US Patent No. 3,966,382).

JP 60-125627 teaches the basic claimed process of injection stretch blow molding of a polypropylene container including, providing a polypropylene based composition having a melt flow index of 4-50 g/10 min, injecting said composition into a mold to form a preform and removing said preform to be blow molded in a subsequent molding step.

Regarding claims 26, 41, 45, JP 60-125627 does not teach a mold fill rate of at least 5 g/sec. However, it is noted that it is well known that the mold fill rate is dependent on the injection pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence it is submitted that the mold fill rate is a result effective variable. Therefore, it would have been obvious for one of ordinary skill in the art to have used routine experimentation in the process of JP 60-125627 to determine an optimum mold fill rate of at least 5 g/sec because it is well known that the mold fill rate is dependent on the injection pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence the mold fill rate being a result effective variable.

Further regarding claims 26, 41, 45, JP 60-125627 does not teach a preform wall thickness of less than 3.5 mm. Edwards ('382) teaches that the wall thickness of a polypropylene preform used in an injection-blow molding process is 0.02 inches (0.5 mm) (see col. 1, line 57 through col. 2, line 15). Therefore, it would have been obvious for one of ordinary skill in the art to have molded a polypropylene preform having a wall thickness of 0.5 mm (less than 3.5 mm) as taught by Edwards ('382) using the process of JP 60-125627 because Edwards ('382) specifically teaches that such a value provides for a highly accurate end-product, hence providing for an improved product.

In regard to claim 39, 42 and 46, JP 60-125627 teaches reheating and stretch-blow molding of the preform to form a container (see Abstract).

Specifically regarding claim 33, although JP 60-125627 in view Edwards ('382) teaches a polypropylene preform wall thickness of 0.5 mm, JP 60-125627 in view Edwards ('382) does not

teach a polypropylene preform wall thickness of 1.5-3.5 mm. However, Edwards ('382) teaches that the preform wall thickness depends on the type of resin, heating temperature, injection pressure. Hence, it is submitted that in view of the teachings of Edwards ('382), it would have been obvious for one of ordinary skill in the art to have used routine experimentation to determine an optimum wall thickness in the process of JP 60-125627 in view Edwards ('382) because, Edwards ('382) teaches that the preform wall thickness depends on the type of resin, heating temperature, injection pressure, hence teaching that the preform wall thickness is a result effective variable.

Regarding claims 32, 35-37, JP 60-125627 in view Edwards ('382) does not teach a mold fill rate of 5-22 g/sec. However, it is noted that it is well known that the mold fill rate is dependent on the injection pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence it is submitted that the mold fill rate is a result effective variable. Therefore, it would have been obvious for one of ordinary skill in the art to have used routine experimentation in the process of JP 60-125627 to determine an optimum mold fill rate of 5-22 g/sec because it is well known that the mold fill rate is dependent on the injection pressure, the resin viscosity, the resin temperature, the back-pressure and the sprue cross-section, hence the mold fill rate being a result effective variable.

Regarding claims 27 and 34, Edwards ('382) teaches a mold gate of about 3 mm (see Figures 2-3).

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6. Claims 30 and 49 are rejected under 35 U.S.C. 103(a) as being unpatentable over JP 60-

125627 in view of Edwards (US Patent No. 3,966,382) and in further view of Schmidt et al.

(US2004/0063830 A1).

JP 60-125627 in view Edwards ('382) teach the basic claimed process as described

above.

Regarding claims 30 and 49, although JP 60-125627 teaches the use of a nucleating

agent, JP 60-125627 in view Edwards ('382) do not teach a specific nucleating agent. However,

the use of a nucleating agent to improve the transparency of the polypropylene molded container

is well known as evidence by Schmidt et al. (US2004/0063830 A1) who teaches the use of a

variety of nucleating agents including the claimed nucleating agents. Therefore, it would have

been obvious for one of ordinary skill in the art to have provided the nucleating agent taught by

Schmidt et al. (US2004/0063830 A1) in the process of JP 60-125627 in view Edwards ('382)

because, Schmidt et al. (US2004/0063830 A1) teaches that a nucleating agent provides for

improved transparency, hence providing for an improved product.

Conclusion

7. The prior art made of record and not relied upon is considered pertinent to applicant's

disclosure.

8. Any inquiry concerning this communication or earlier communications from the

examiner should be directed to Stefan Staicovici, Ph.D. whose telephone number is (571) 272-

1208. The examiner can normally be reached on Monday-Friday 9:30 AM to 6:00 PM.

If attempts to reach the examiner by telephone are unsuccessful, the examiner's

supervisor, Michael P. Colaianni, can be reached on (571) 272-1196. The fax phone number for

the organization where this application or proceeding is assigned is 571-273-8300.

Information regarding the status of an application may be obtained from the Patent

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system, contact the Electronic Business Center (EBC) at 866-217-9197 (toll-free).

Stefan Staicovici, PhD

Primary Examiner

AU 1732

September 23, 2005